



# Challenges in Managing Mercury in Field Development and Production

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### Challenges in Managing Mercury in Field Development and Production



# **Enhancing Sulfur Efficacy in Mercury Removal from**Natural Gas Condensate and Produced Water

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### Introduction – it is possible to utilize aqueous sulfides to elicit mercury removal in hydrocarbon matrices



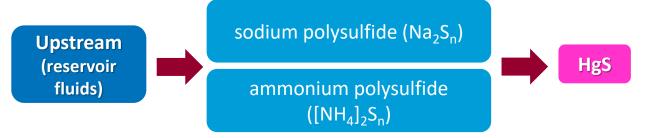
**Literature**; use of aqueous polysulfide solutions can effectively react with mercury compounds at near room temperature to form HgS;

Elemental Hg : 
$$Hg^0 + S^{2-}_n \rightarrow HgS + S^{2-}_{n-1}$$

Organic Hg : 
$$R-Hg-R' + S^{2-}_{n} \rightarrow HgS + S^{2-}_{n-1} + R-R'$$

Inorganic Hg : 
$$HgCl_2 + S^{2-}_n \rightarrow HgS + S^{2-}_{n-1} + 2Cl^{-}$$

**Patents**; upstream processes; sodium polysulfide ( $Na_2S_n$ ) and ammonium polysulfide ( $Na_2S_n$ ) utilized for reducing mercury concentrations in reservoir fluids to below 100 ppb (wt).



Percent mercury removal / %				
Aqueous sulfides		Hg species		
		Hg <sup>0</sup> condy	HgCl <sub>2condy</sub>	Hg(NO <sub>3</sub> ) <sub>2PW</sub>
Na <sub>2</sub> S	Onshore	33	24	95
	Offshore	52	38	88
(NH <sub>4</sub> ) <sub>2</sub> S	Onshore	40	50	93
	Offshore	25	23	87
K <sub>2</sub> S	Onshore	33	9	94
	Offshore	33	33	64

**NOTE** Ratio of [mercury species] to [aq. sulfide] is ca. 1:1.

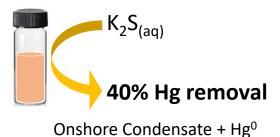
- Aqueous sulfides are effective in removing mercury(II) from produced water (PW)
- Also shows ability to remove mercury from condensate (condy)

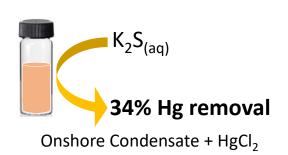
**Source**: i. Yan, T. Y. Mercury Removal from Oils. Chem. Eng. Commun. 2000, 177 (Oct. 2014), ii. Yan, T. Y. US 4,915,818 Use of Dilute Aqueous Solutions of Alkali Polysulfides to Remove Trace Amounts of Mercury from Liquid Hydrocarbons (1990), iii. Yean, S.; Gallup, D. L.; Young, L. A.; Cooper, R. E.; Zielinski, M. B.; Emanuele, A.; Llewellyn, B. C.; O'rear, D. J. US 9,447,675 B2 In-Situ Method and System for Removing Heavy Metals from Produced Fluids (2016), iv. Wong, S.M.A.S and Salam, S. IPTC-24982-MS: Enhancing Mercury Removal in Hydrocarbon Fluids: Efficacy of Aqueous Sulfides Extraction in Natural Gas Condensate and Produced Water, Internat. Petroleum. Tech. Conf., Kuala Lumpur (Feb. 2025).

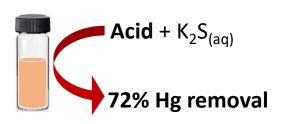


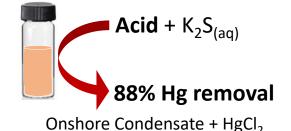
### The use of an acid together with an aqueous sulfide improves the Hg removal in condensate samples











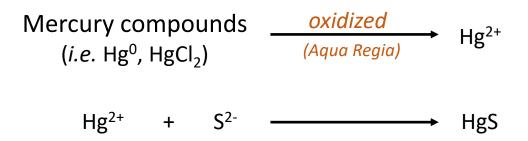
Onshore Condensate + Hg<sup>0</sup>

(Increase of ca. 32%)

(Increase of ca. 54%)

#### **NOTE**

- i. Sample matrix: onshore condensate, with initial  $[Hg^0, HgCl_2] = 3,000 \text{ ppb wt.}$
- ii. Ratio of S<sup>2-</sup> to Hg<sup>2+</sup> was 1.7:1 (excess sulfides)

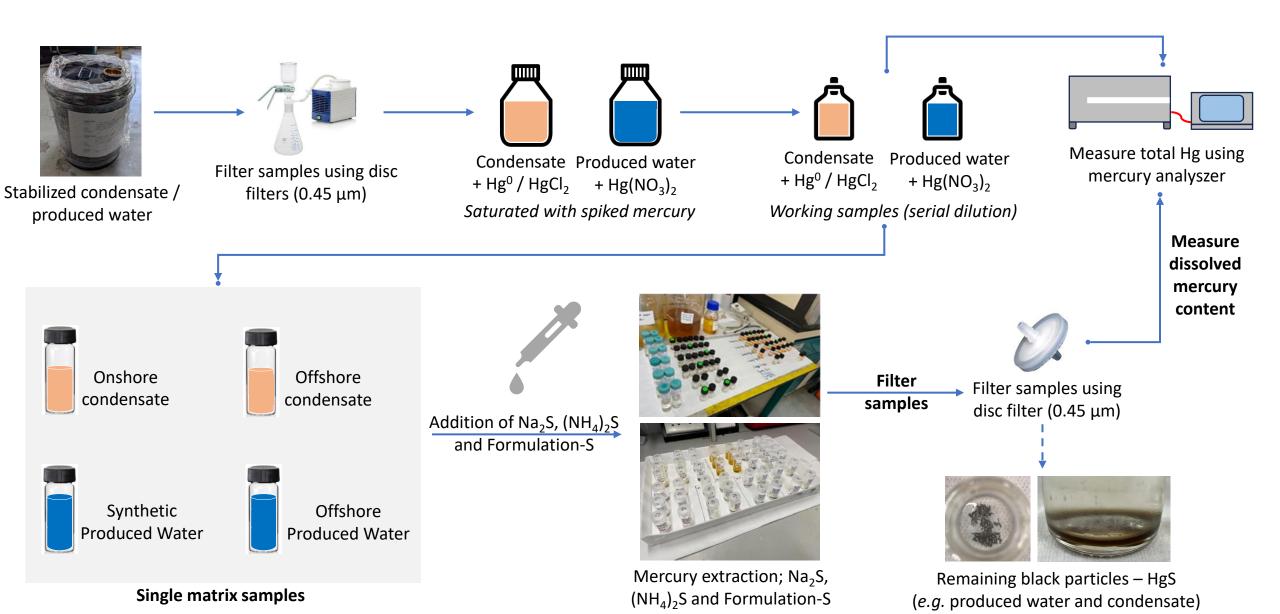


- Oxidant (i.e. Aqua Regia) enhances mercury extraction by oxidizing Hg<sup>0</sup> and HgCl<sub>2</sub> to Hg<sup>2+</sup>, followed by complexation with S<sup>2-</sup> to form HgS. Oxidants are widely used for mercury extraction (e.g. acid digestion) in standard methods (e.g. EPA, ISO).
- Improving Hg<sup>2+</sup> availability before sulfide complexation enhances mercury extraction efficiency.
- However, introducing acids into process streams is impractical due to operational and safety concerns.
- Sulfide that is capable of performing oxidation without the need of an acid; Formulation-S



#### Experimental workflow: Sample preparation, Hg removal tests, and total mercury analysis (n ≥ 2)

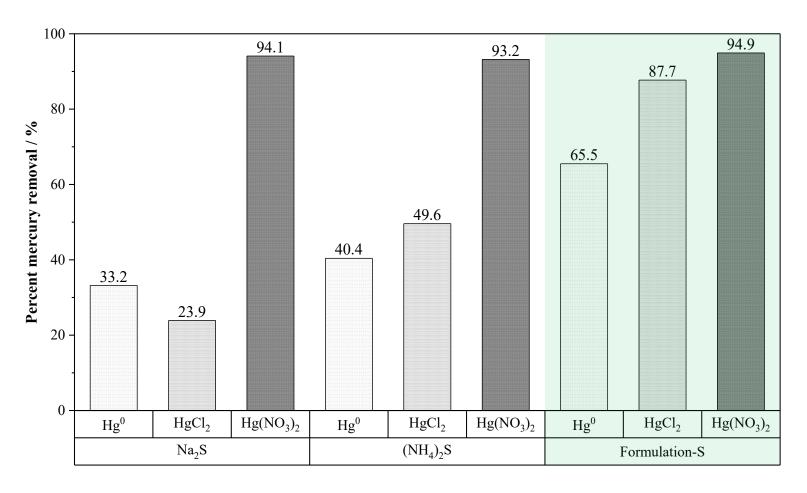






# Onshore sample set: Formulation-S resulted in highest overall Hg removal vs aqueous sulfides (Na<sub>2</sub>S, (NH<sub>4</sub>)<sub>2</sub>S)





#### Order of percent Hg mercury removal

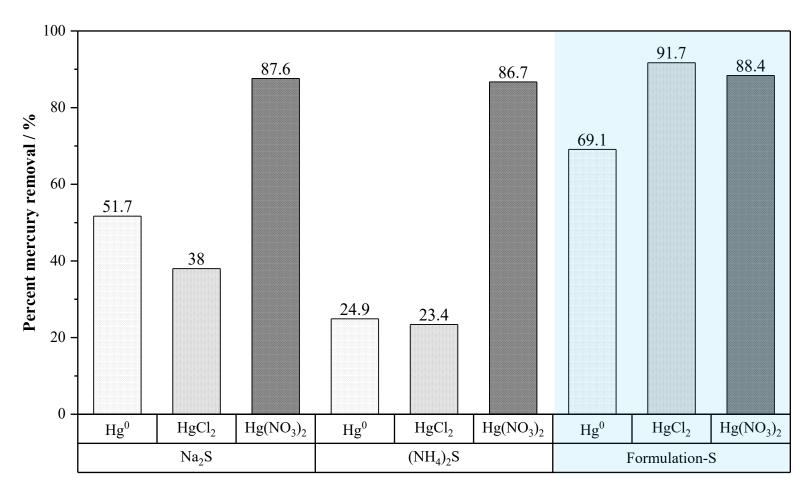
- Hg<sup>0</sup> in condensate
  - $F-S > (NH_4)_2S > Na_2S$
- HgCl<sub>2</sub> in condensate
  - $\rightarrow$  F-S > (NH<sub>4</sub>)<sub>2</sub>S > Na<sub>2</sub>S
- Hg(NO<sub>3</sub>)<sub>2</sub> in syn. prod. water
  - ightharpoonup F-S > Na<sub>2</sub>S > (NH<sub>4</sub>)<sub>2</sub>S
- Both F-S and aq. sulfides show
  - high level of Hg<sup>2+</sup> removal in syn. prod. water,
  - but varying levels of removal in condensate,

Percent mercury removal in **onshore condensate** (single-matrix) containing  $Hg^0$  and  $HgCl_2$ , and **synthetic produced** water containing  $Hg(NO_3)_2$ . Results adjusted to account for mercury loss. Initial mercury concentration for each sample was ca. 1,000 ppb wt. Each percentage represents a samples size  $n \ge 2$ .



# Offshore sample set: Formulation-S resulted in highest overall Hg removal vs aqueous sulfides (Na<sub>2</sub>S, (NH<sub>4</sub>)<sub>2</sub>S)





#### Order of percent Hg mercury removal

- Hg<sup>0</sup> in condensate
  - ightharpoonup F-S > Na<sub>2</sub>S > (NH<sub>4</sub>)<sub>2</sub>S
- HgCl<sub>2</sub> in condensate
  - ightharpoonup F-S > Na<sub>2</sub>S > (NH<sub>4</sub>)<sub>2</sub>S
- Hg( $NO_3$ )<sub>2</sub> in syn. prod. water
  - ightharpoonup F-S > Na<sub>2</sub>S > (NH<sub>4</sub>)<sub>2</sub>S
- Both F-S and aq. sulfides show
  - high level of Hg<sup>2+</sup> extraction in syn. prod. water,
  - but varying levels of extraction in condensate,
- Similar trend observed with the onshore sample set.

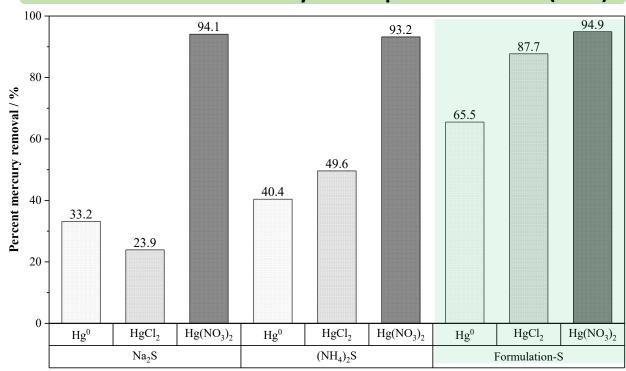
Percent mercury removal in **offshore condensate** (single-matrix) containing  $Hg^0$  and  $HgCl_2$ , and **offshore produced** water containing  $Hg(NO_3)_2$ . Results adjusted to account for mercury loss. Initial mercury concentration for each sample was ca. 1,000 ppb wt. Each percentage represents a samples size  $n \ge 2$ .



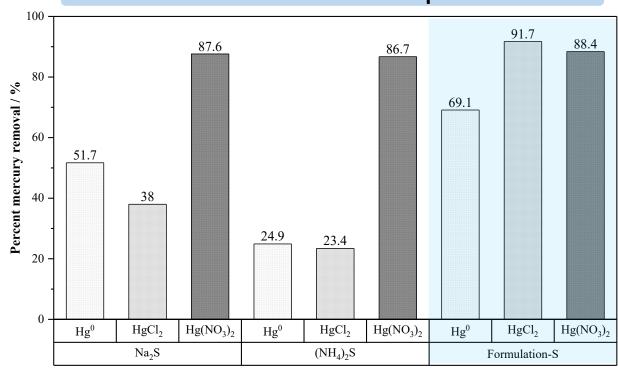
### Formulation-S resulted achieved highest overall Hg removal for both onshore and offshore sample sets



#### Onshore condensate and synthetic produced water (SPW)



#### Offshore condensate and offshore produced water

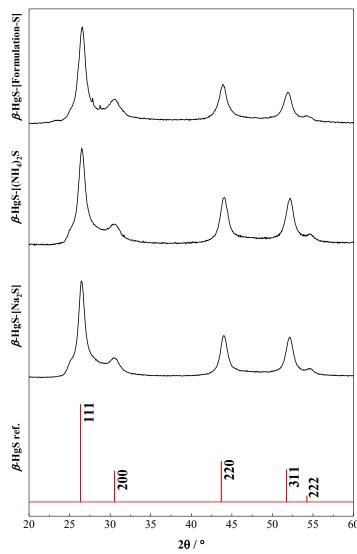


Percent mercury removal in **onshore/offshore condensate** (single-matrix) containing  $Hg^0$  and  $HgCl_2$ , and **synthetic/offshore produced water** containing  $Hg(NO_3)_2$ . Results adjusted to account for mercury loss. Initial mercury concentration for each sample was ca. 1,000 ppb wt. Each percentage represents a samples size  $n \ge 2$ .

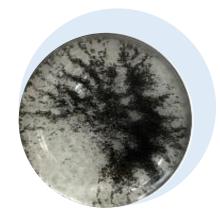


### Black precipitates formed in solution post mercury removal was identified as $\beta$ -HgS (metacinnabar)





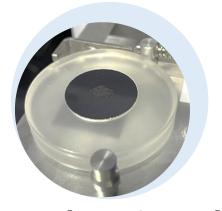
Diffractogram of black precipitates isolated from treatment of solution containing  $Hg(NO_3)_2$ .



 $\beta$ -HgS-[Na<sub>2</sub>S]



 $\beta$ -HgS-[(NH<sub>4</sub>)<sub>2</sub>S]



**β-HgS-[Formulation-S]**Pictured here on zero
background sample holder

 $\triangleright$  All 3 diffractograms was **matched** to powder diffraction file of  $\beta$ -HgS – PDF 00-006-0261 (star quality) obtained from ICDD and exhibits cubic (zinc blende) phase of **metacinnabar**.

**NOTE** Cinnabar ( $\alpha$ -HgS), red HgS, exhibits hexagonal phase.

 $\triangleright$  2 main polymorphs of mercury(II) sulfide exist;  $\alpha$ -HgS (red) and  $\beta$ -HgS (black). The metacinnabar variant results from precipitation.

**Source:** i. Simon, M.; Jonk, P.; Wuhl-Couturier, G.; Daunderer, M. Handbook of Extractive Metallurgy Chapter 17; Habashi, F., Ed.; Wiley-VCH (1997) Vol. Volume 2. ii. Wong, S.M.A.S and Salam, S. IPTC-24982-MS: Enhancing Mercury Removal in Hydrocarbon Fluids: Efficacy of Aqueous Sulfides Extraction in Natural Gas Condensate and Produced Water, Internat. Petroleum. Tech. Conf., Kuala Lumpur (Feb. 2025).



#### **Summary and conclusion**



- Formulation-S was able to attain mercury removal of
  - ➤ 65-69% (Hg<sup>0</sup>) in condensate,
  - ➤ 88-92% (HgCl<sub>2</sub>) in condensate,
  - $\triangleright$  88-95% (Hg(NO<sub>3</sub>)<sub>2</sub>) in produced water,
- The formulation was able to remove mercury from both hydrocarbon and water matrices, suggesting it was **able to disperse/miscible in both matrices**,
- Black precipitants were observed to have formed via precipitation in treated samples,
- The black precipitate was identified to be **mercury(II) sulfide** (i.e. metacinnabar) from XRD analysis,
- This suggest the presence of a **reactive sulfide** species that is capable of performing oxidative complexation with the mercury species present in the sample matrix,
- The formulation can potentially be applied for bulk-removal of mercury.
- Room for further development and testing.





#### Thank you